

## Assessment of Hydrocarbon Explosion and Fire Risks

by

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The LRET Research Collegium  
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**Assessment of Hydrocarbon Explosion and Fire Risks  
in Offshore Installations:  
Recent Advances and Future Trends**

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The LRET Research Center of Excellence  
at Pusan National University, Korea**

# New Paradigm for Robust Design of Ships and Offshore ...

## Various Ocean Environmental Phenomena

Traditional

Design Formula

Past Experience

Deterministic

Allowable Stress

Mathematical Algorithm

$$\sum_{i=1}^m \sum_{j=1}^n \phi \alpha \beta \gamma \lim_{x \rightarrow \infty} \frac{\zeta}{\sqrt{x^2 - \epsilon x + \eta}} \frac{n!}{r!(n-r)!}$$


Future

Engineering

First Principles

Probabilistic

Limit States/Risk

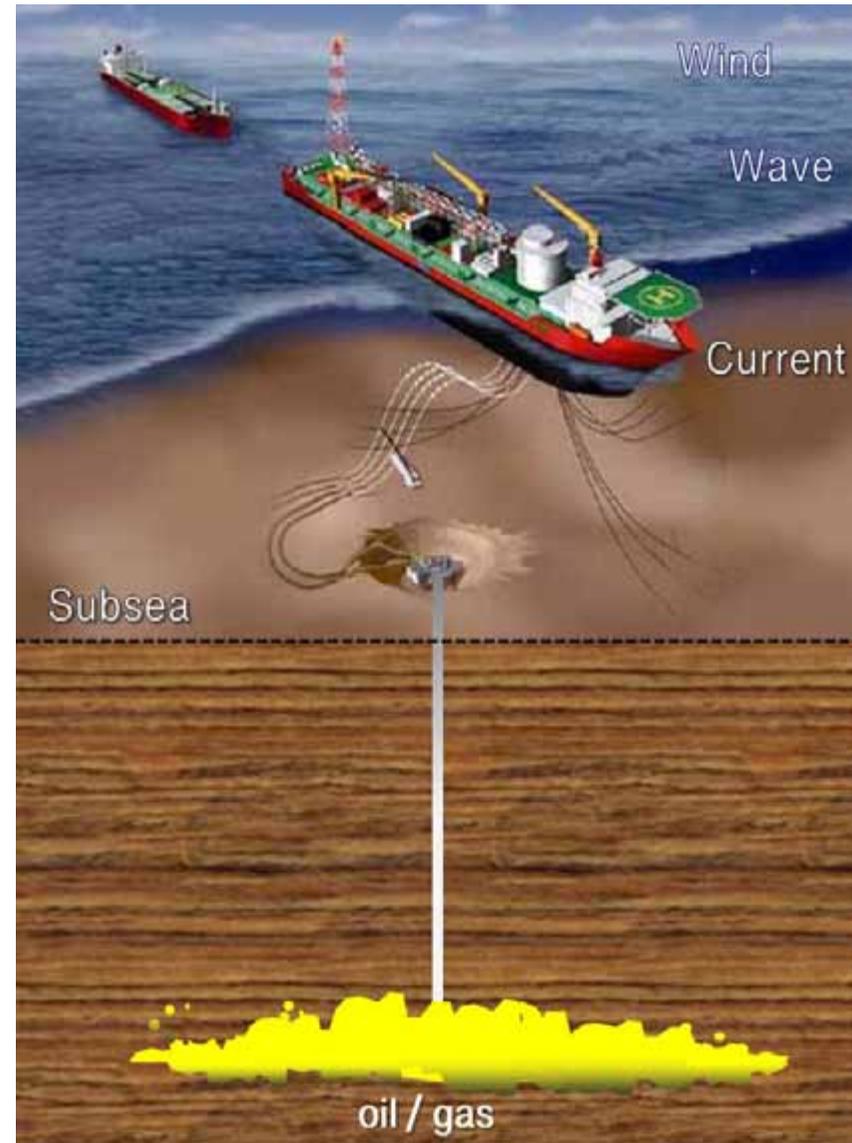
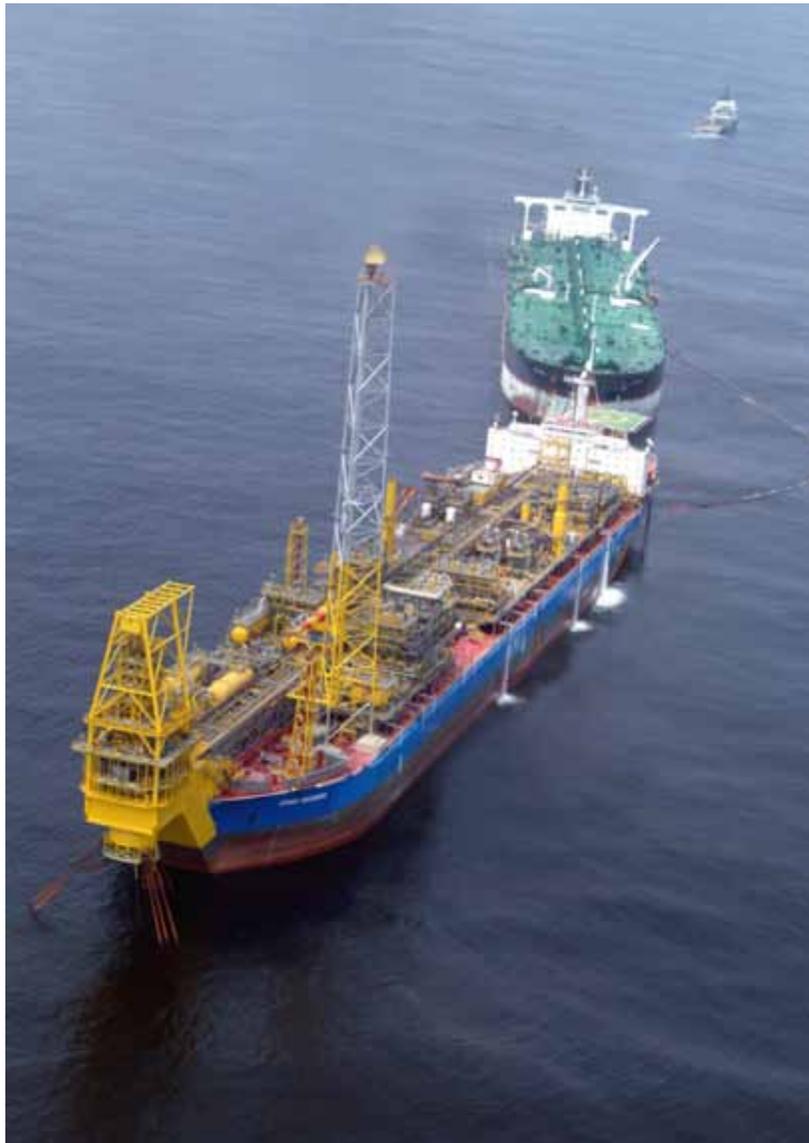
Experimental Investigation

## Trend in Offshore Oil & Gas Production Systems

- Fixed type in shallow waters → Floating type in deep waters
- Ship-shaped offshore unit, Semi-sub, Spar, TLP
- Pipeline infrastructure → Multiple functions such as production, storage and offloading

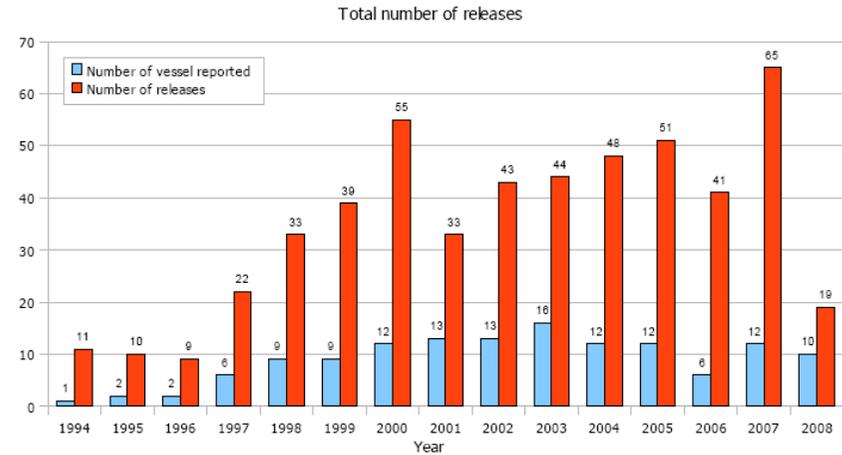
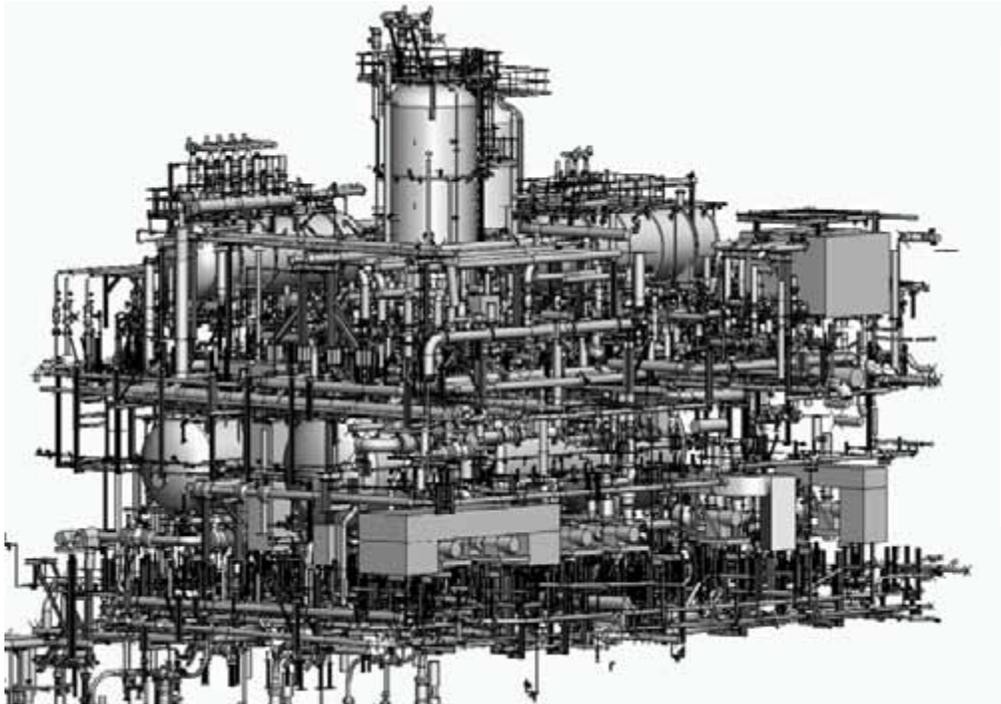


# FPSO for Oil and Gas Production



Vessel (hull), topsides (process facility), mooring, risers/flow lines, subsea, and export system

# Oil/Gas Leak Resulting in Explosion and Fire



Source: HSE



# Pipe Alpha Accident

- 6<sup>th</sup> July 1988, UK
- 167 people killed
- Property damage of 1.4billion US\$
- Risk based engineering became mandatory since the Pipe Alpha accident



# Deepwater Horizon Accident

- 20<sup>th</sup> April 2010, Gulf of Mexico
- 11 people killed, 17 people wounded
- Environmental damage of approx. 30 billion US\$

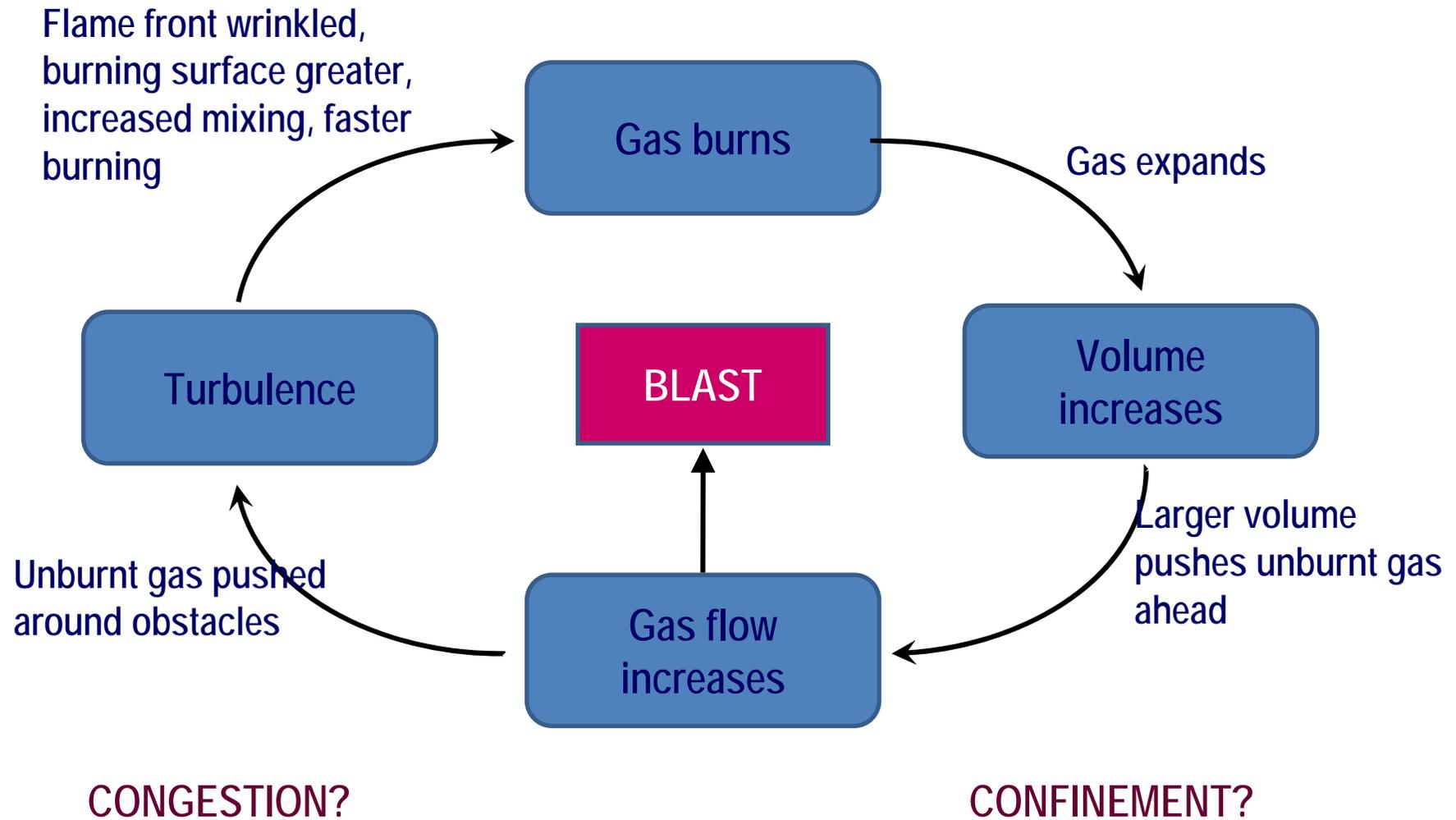


Oil spill

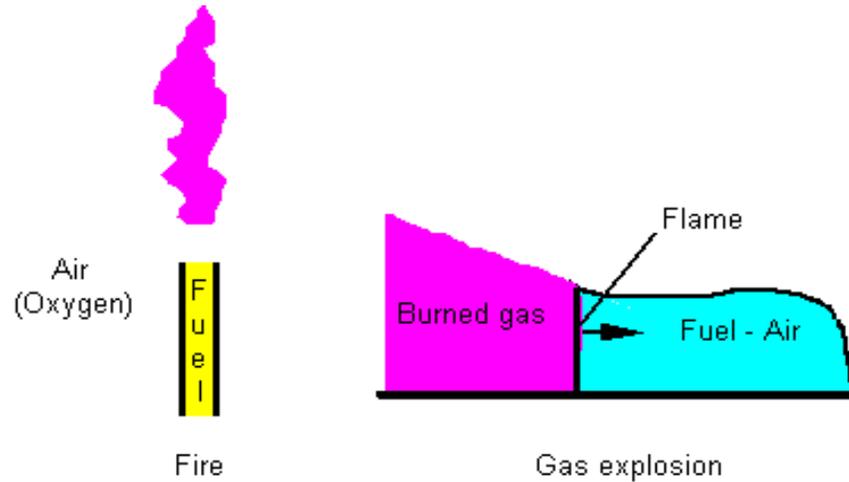
# Hydrocarbon Explosions and Fires

- Hydrocarbons can explode through ignition when combined with an oxidiser (usually air). Thus, when the temperature rises to the point at which hydrocarbon molecules react spontaneously to an oxidiser, combustion takes place. This hydrocarbon explosion causes a blast and a rapid increase in overpressure.
- Fire is a combustible vapour or gas that combines with an oxidiser in a combustion process that is manifested by the evolution of light, heat, and flame.
- The impact of overpressure from explosions and that of elevated temperature from fire are the primary concern in terms of the actions that result from hazards within the risk assessment and management framework.

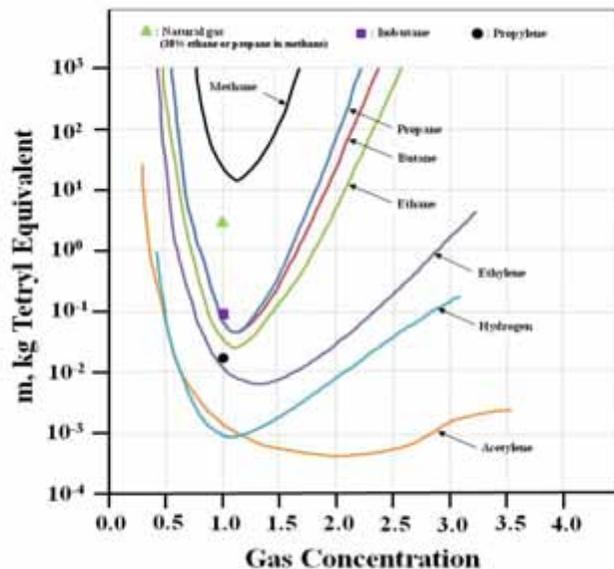
# Mechanism of Gas Explosion – Depending on Topology and Geometry



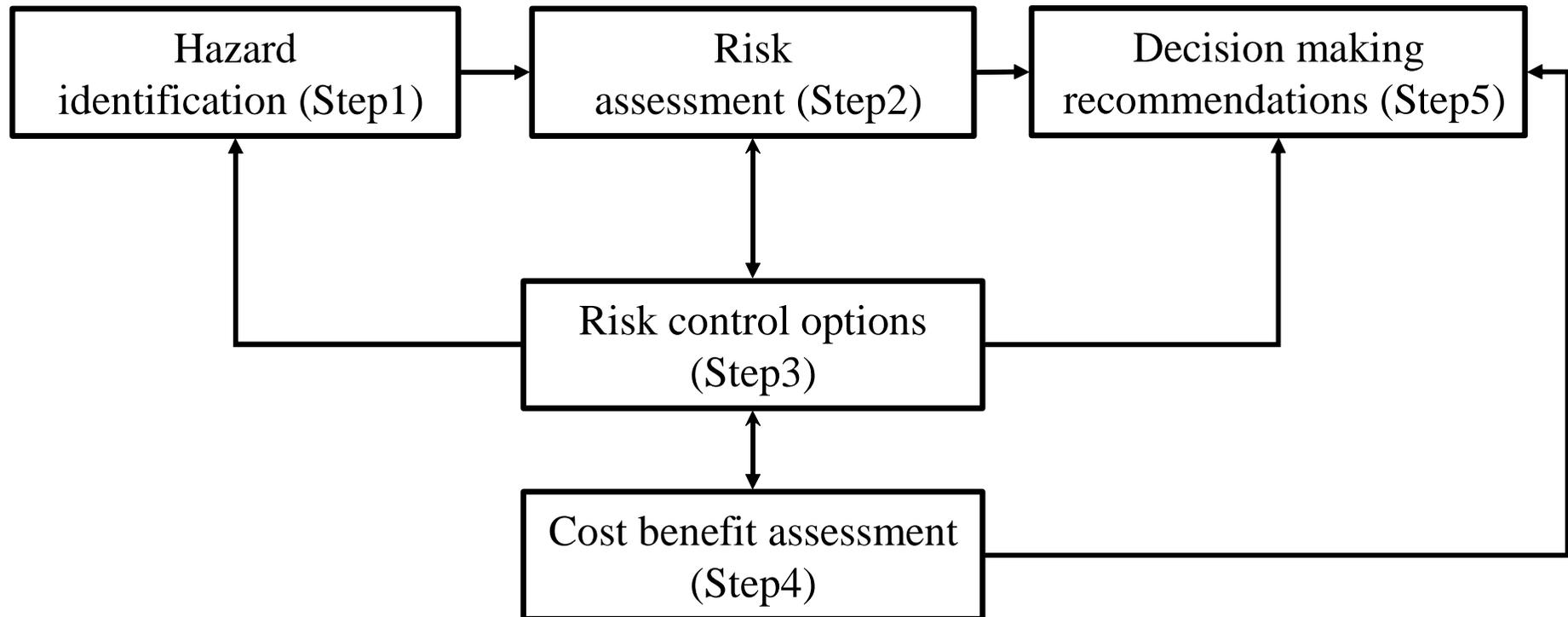
# Factors Affecting Explosions and Fires



- Wind direction
- Wind speed
- Leak rate
- Leak direction
- Leak duration
- Leak position (x)
- Leak position (y)
- Leak position (z)
- Type of oil or gas (molecules)
- Concentration ratio
- Temperature of oil or gas  
(LNG Cryogenic -163 degree C)



# Risk Based Design Process

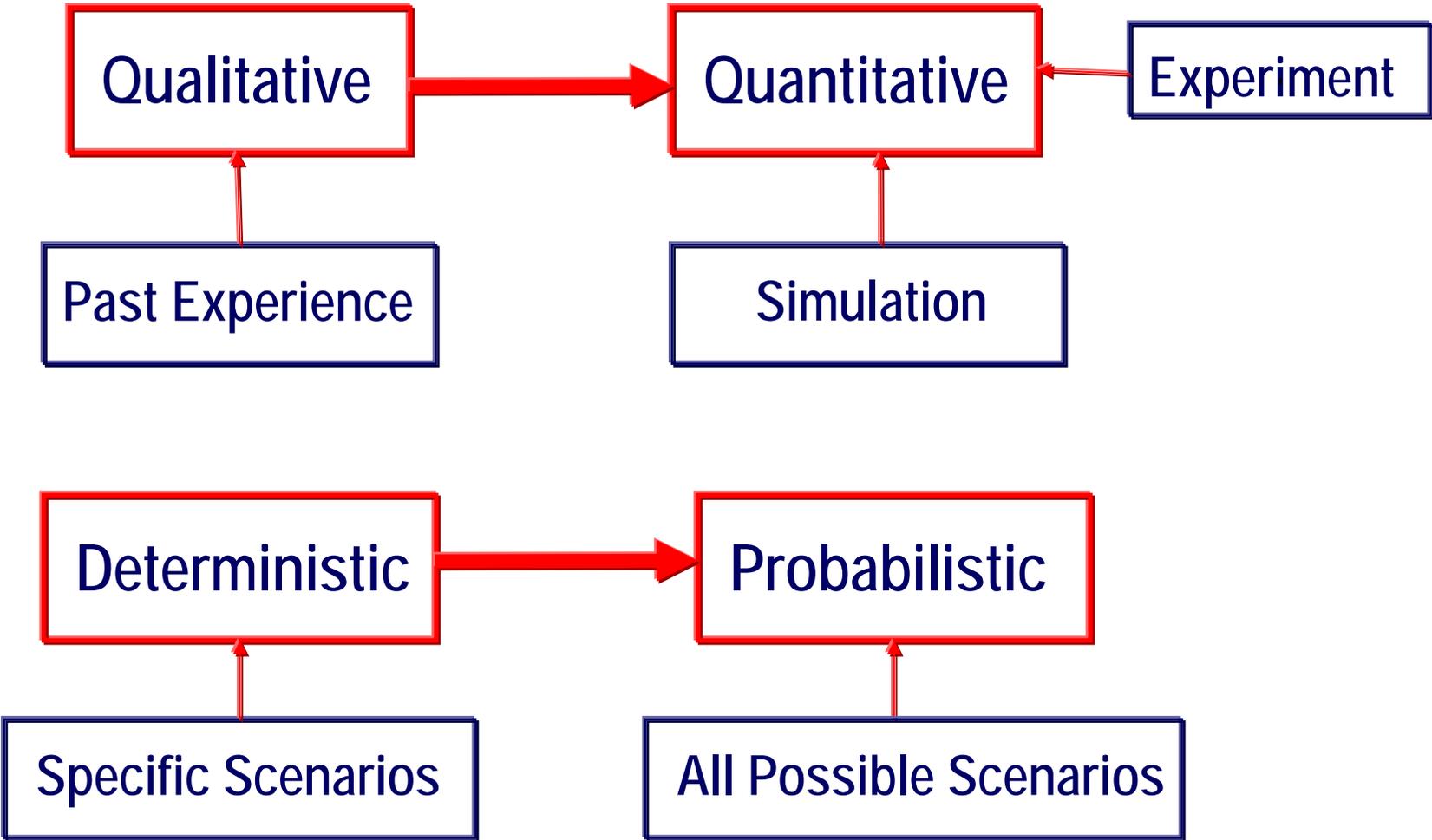


## What is Risk? How to Manage Risk?

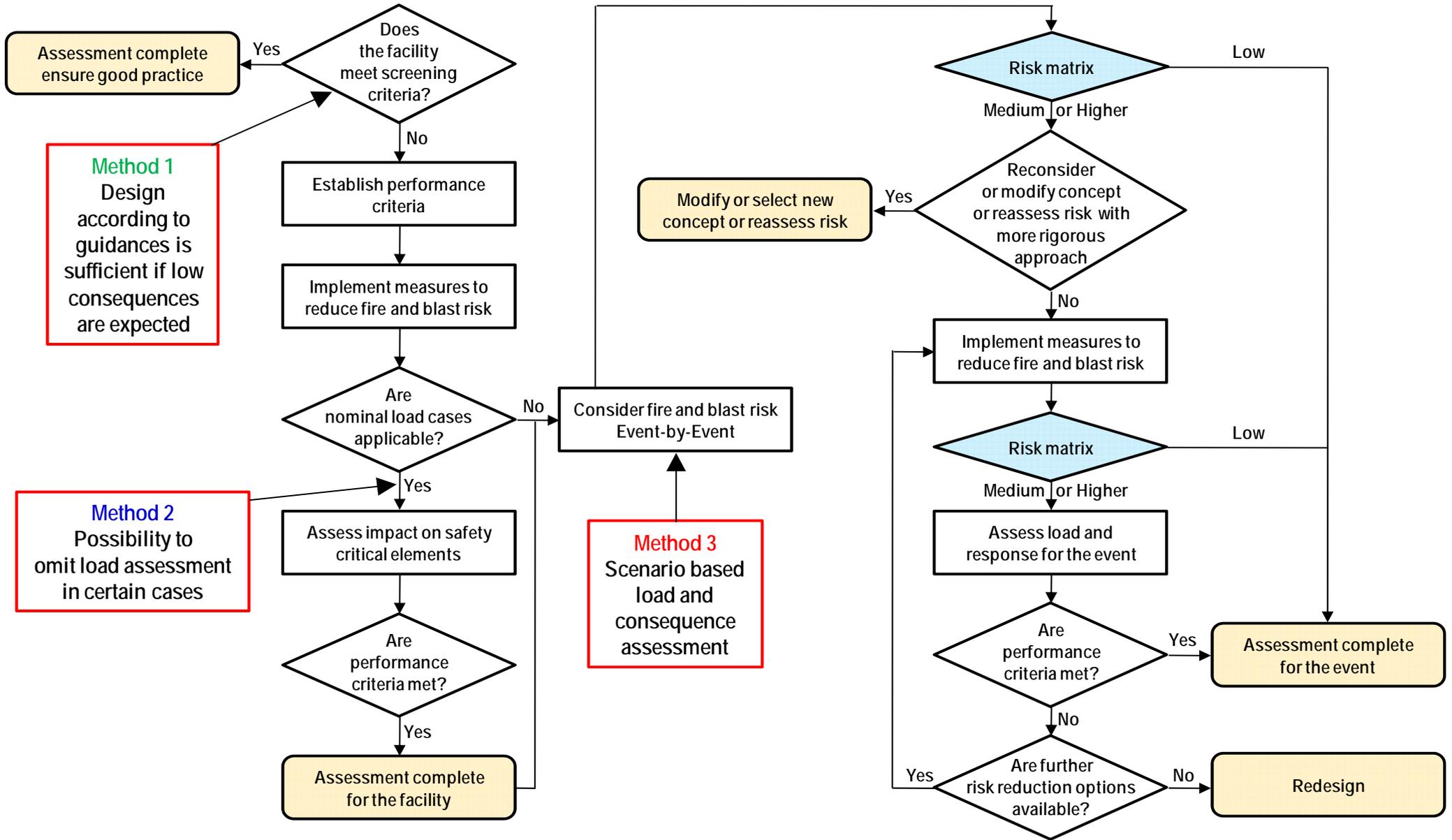
$$R = \sum_i F_i \times C_i$$

- Asset risk
  - Damage to structures and equipment
  - Duration of production delay (downtime)
- Environmental risk
  - Amount of oil that spills out of the offshore installation
- Personnel risk
  - Loss of life

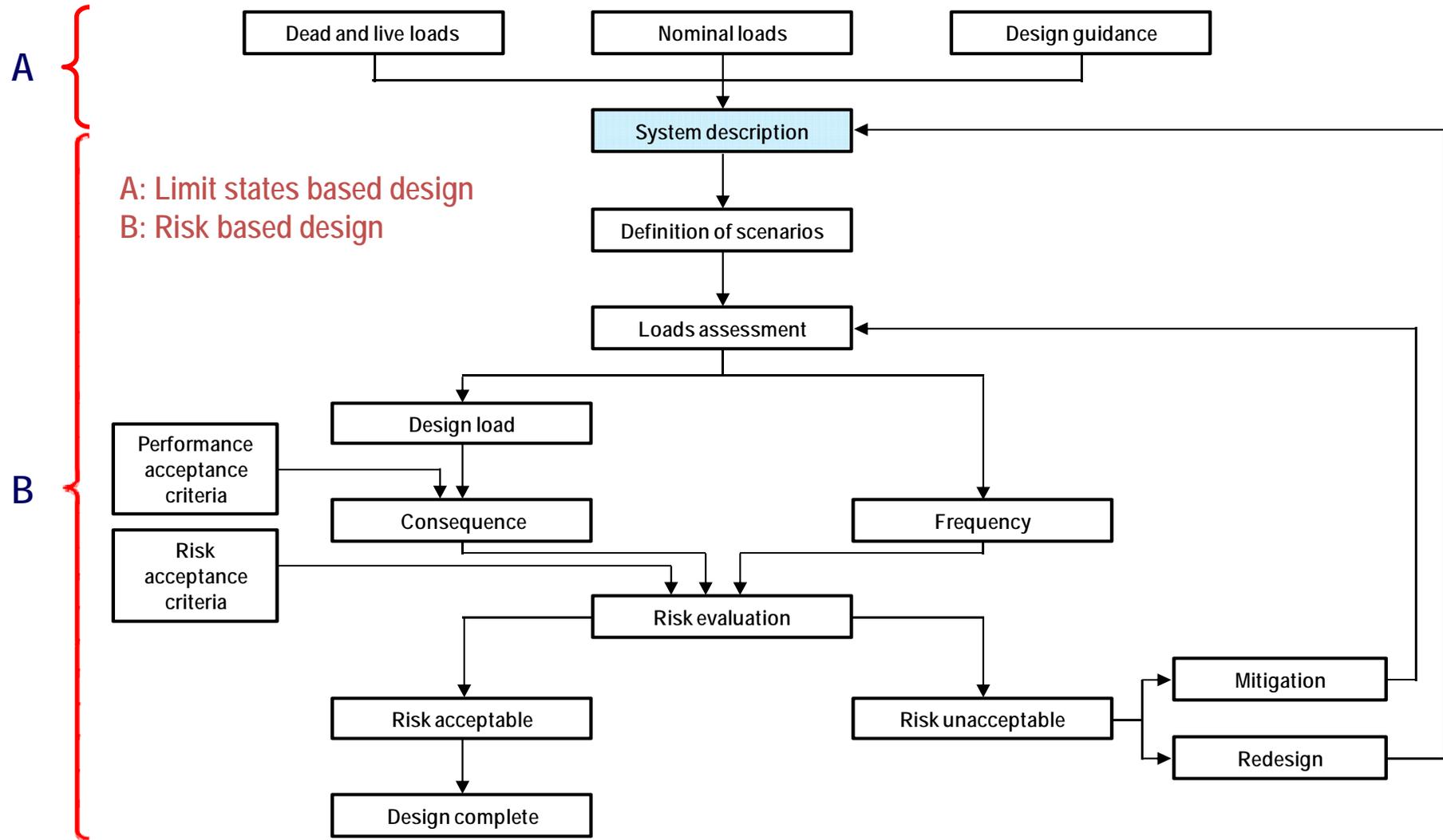
# Trends in Risk Assessment



# API Procedure for Risk-based Design



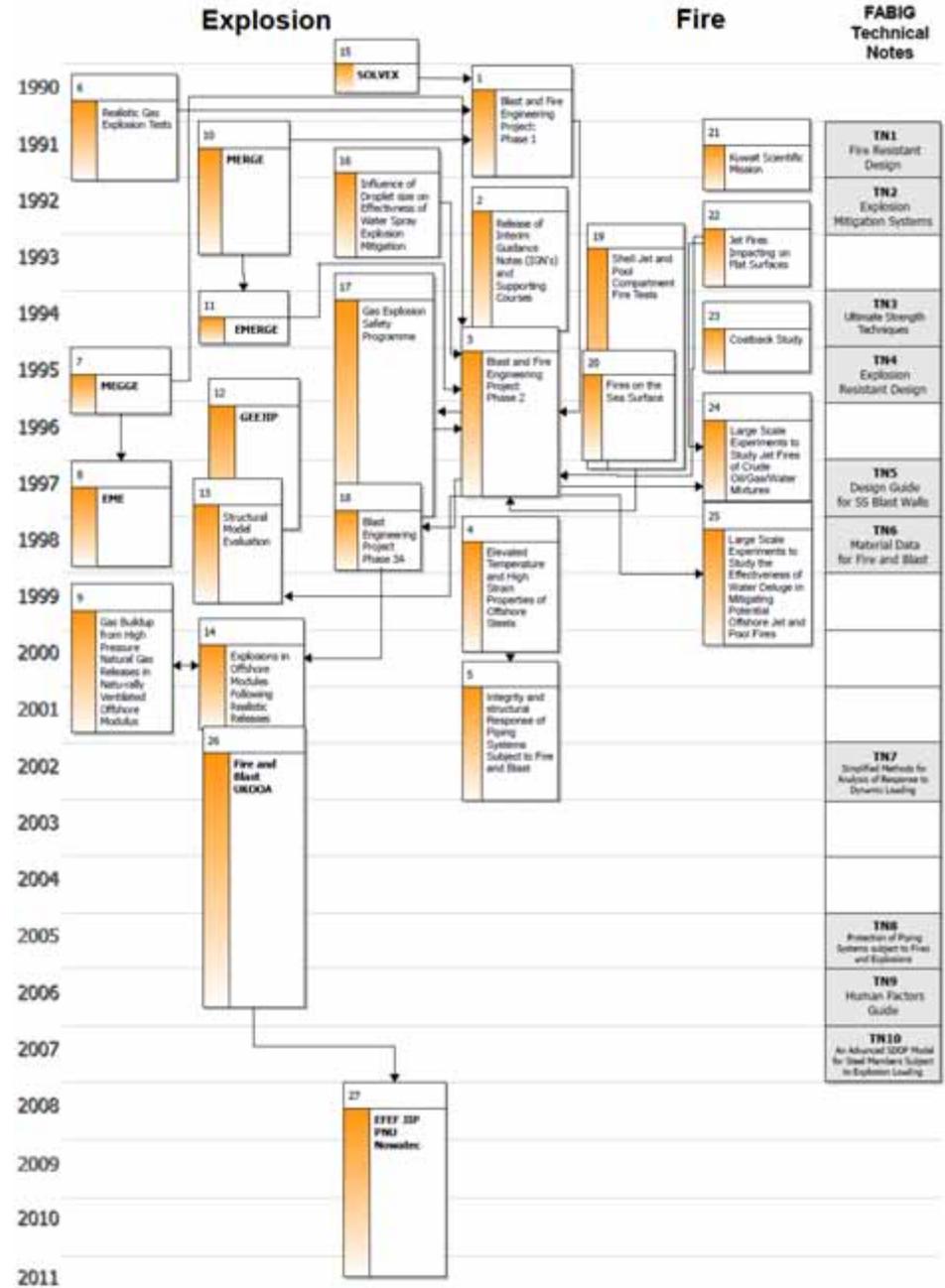
# Simulation-based Procedure for Risk-based Design



# Joint Industry Projects



## Key Explosion and Fire Research Project



# EFEF JIP - 27th JIP in the World

## Explosion and Fire Engineering of FPSOs

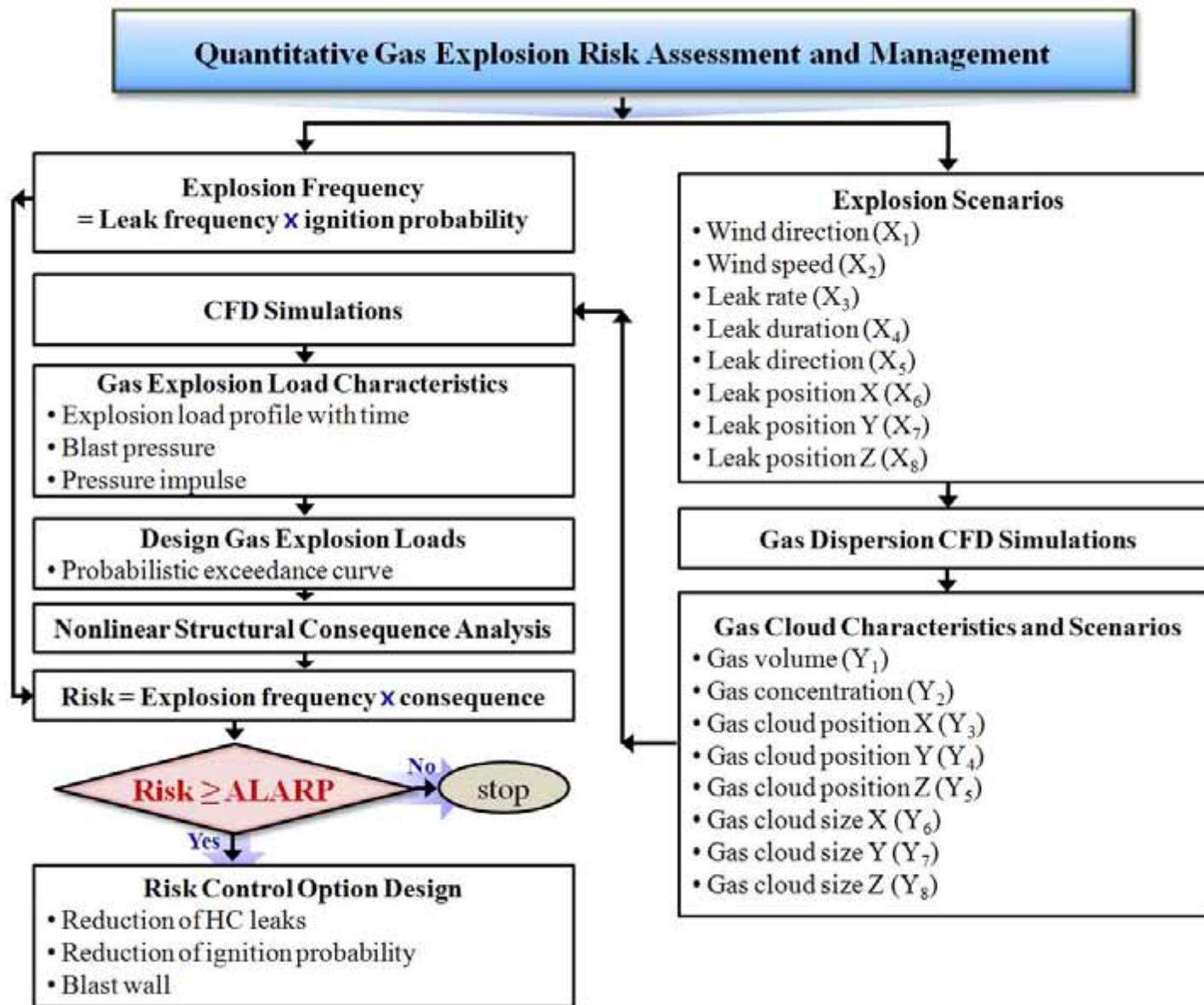
### Coordinators:

- Pusan National University, Korea
- Nowatec AS, Norway

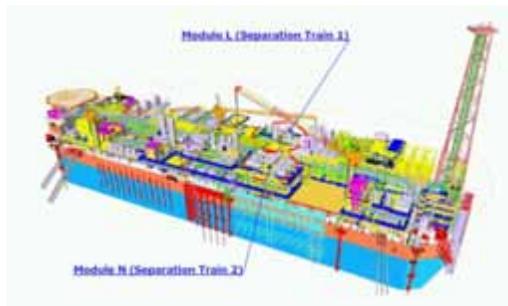
### Partners:

- DSME, SHI, HHI, ABS, KR, LR
- Gexcon, Comput, USFOS, UK HSE, NTUA

# Quantitative Gas Explosion Risk Assessment and Management (1/2)



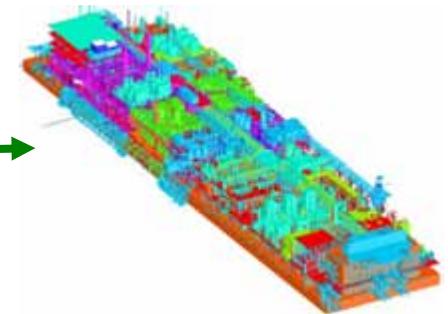
# EFEF JIP Procedure for Explosion Risk Assessment and Management (2/2)



CAD model

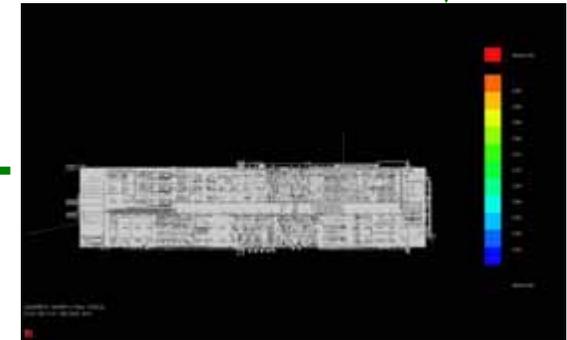
Selection of credible scenarios involving PDF parameters of leak and environment conditions

Latin hypercube sampling technique

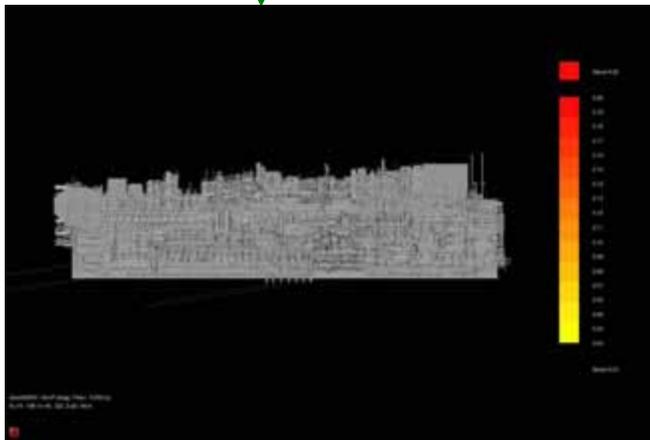


CFD model

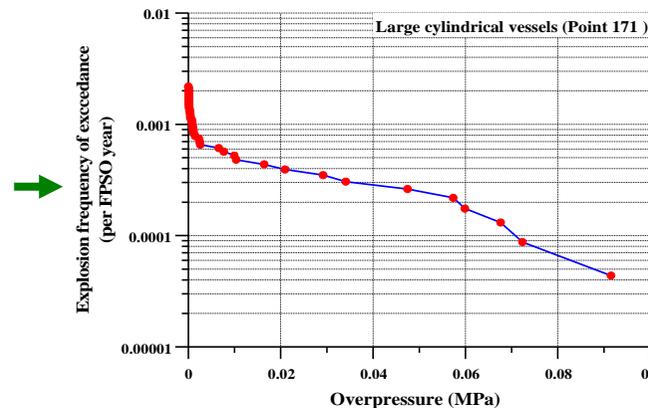
Selection of credible scenarios involving PDF parameters of gas cloud condition



Gas dispersion analysis



Explosion CFD simulation

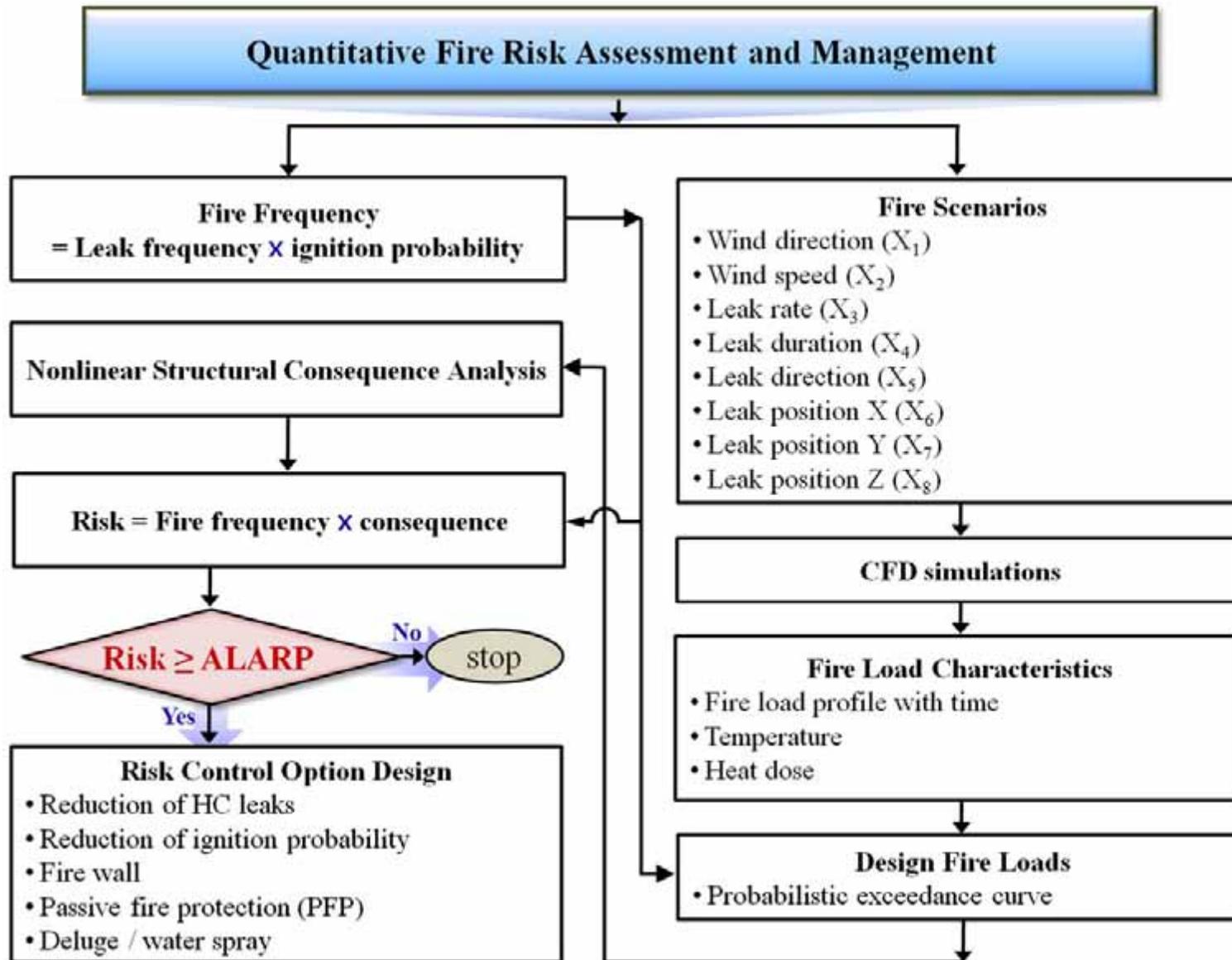


Design loads with exceedance curve

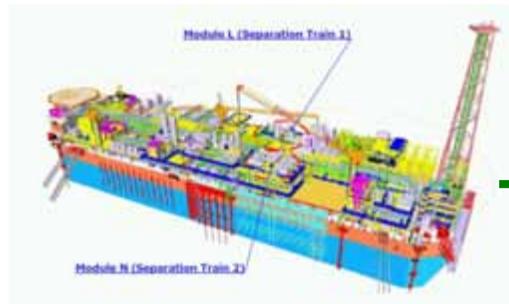


Nonlinear consequence analysis under explosion

# EFEF JIP Fire Risk Assessment and Management (1/2)



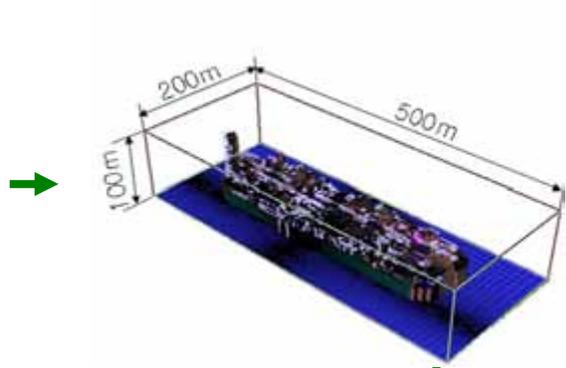
# EFEF JIP Procedure for Fire Risk Assessment and Management (2/2)



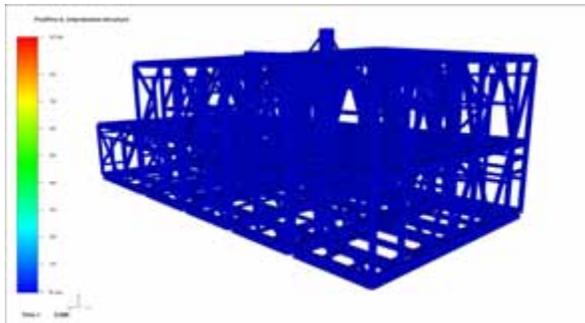
CAD model

Selection of credible scenarios involving PDF parameters of leak and environment conditions

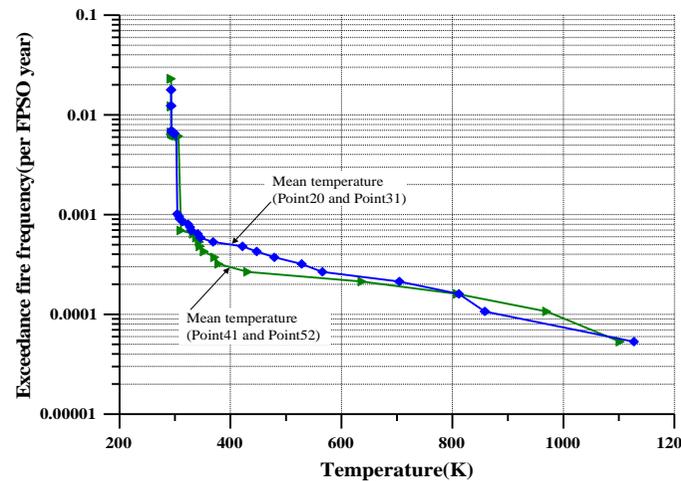
Latin hypercube sampling technique



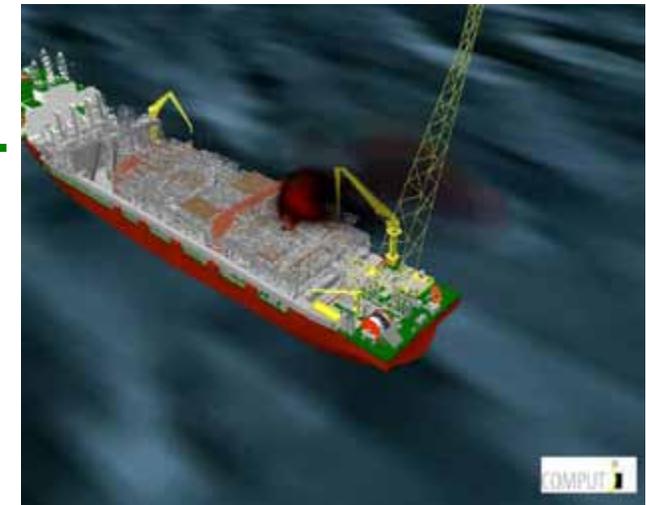
CFD model



Nonlinear consequence analysis under fire

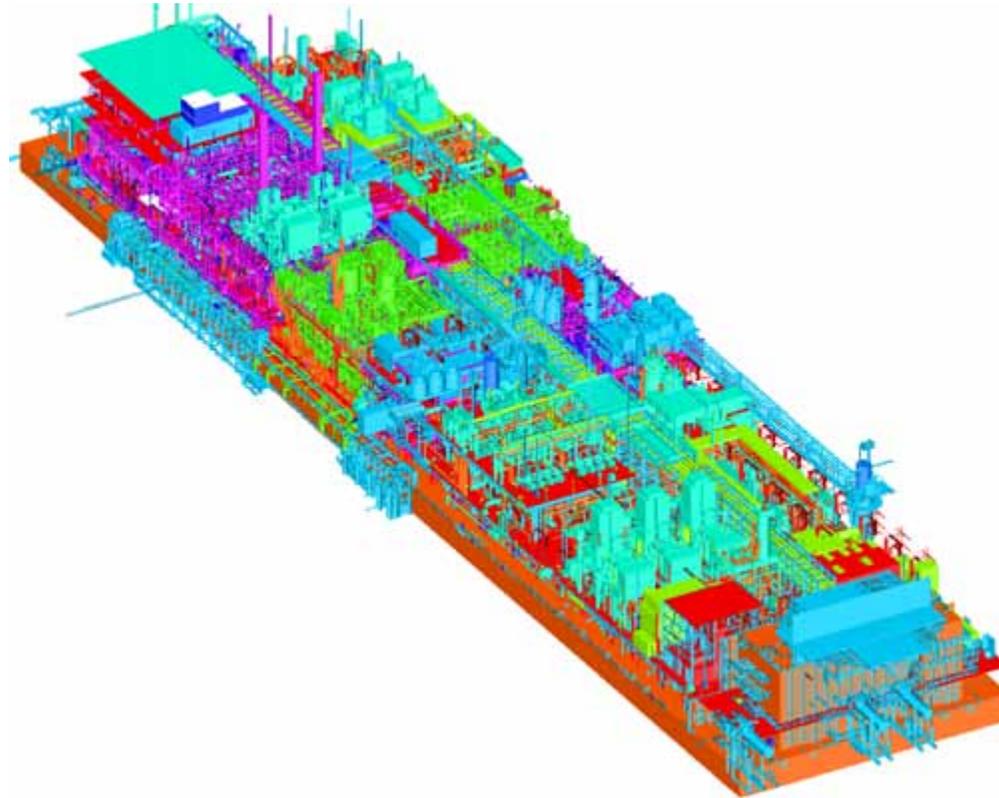
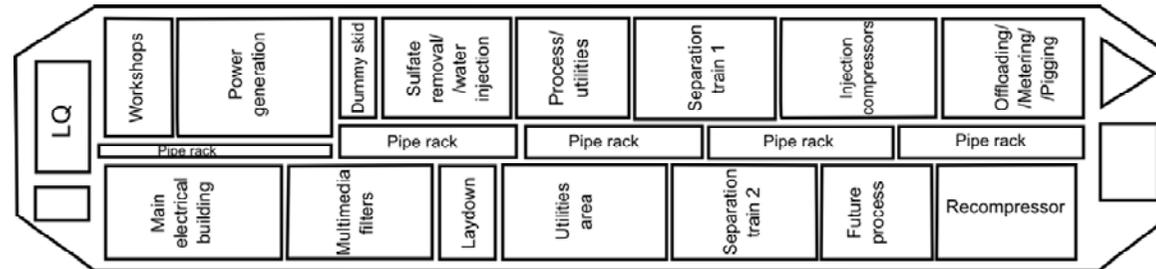


Design loads with exceedance curve

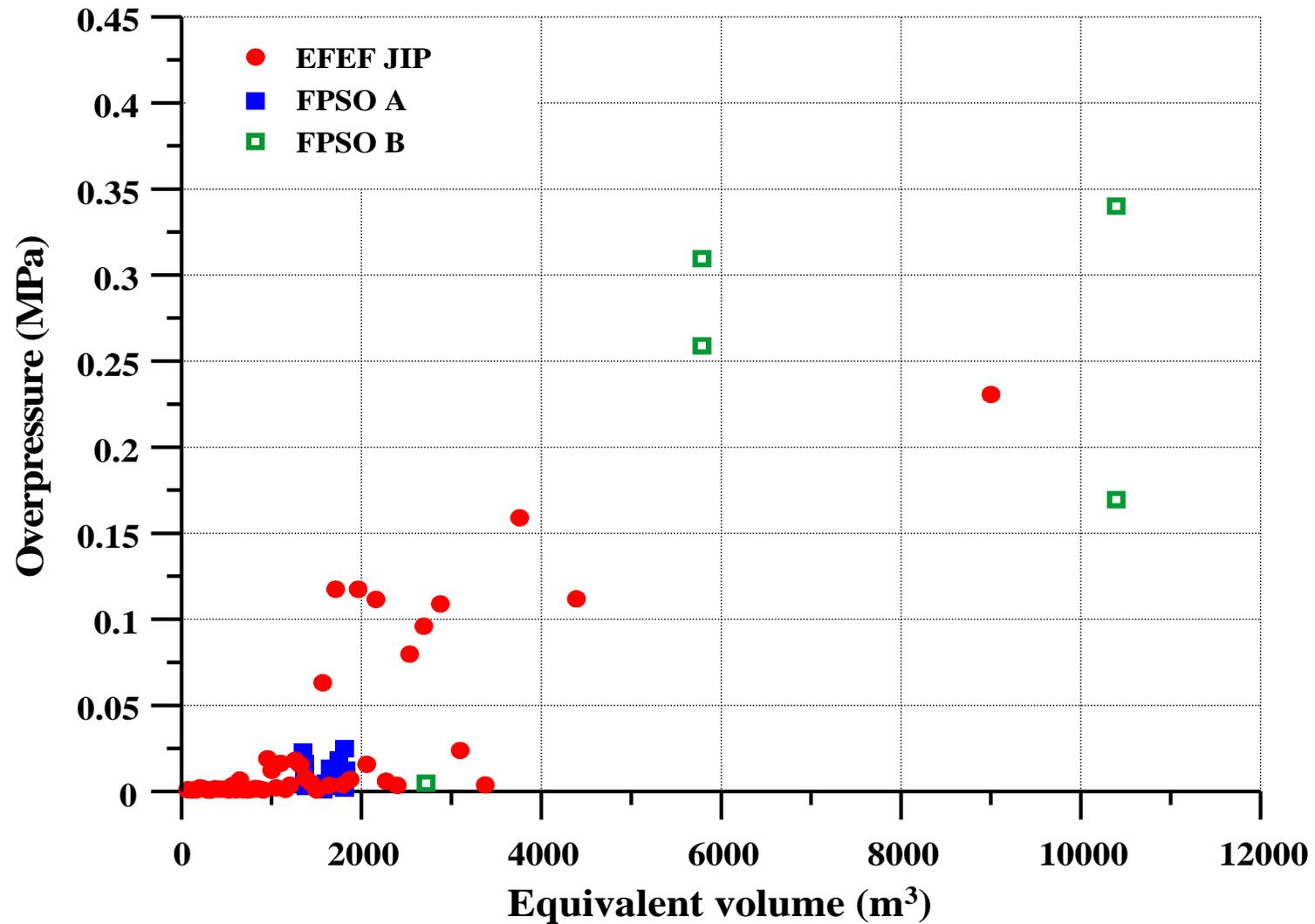


Fire CFD simulation

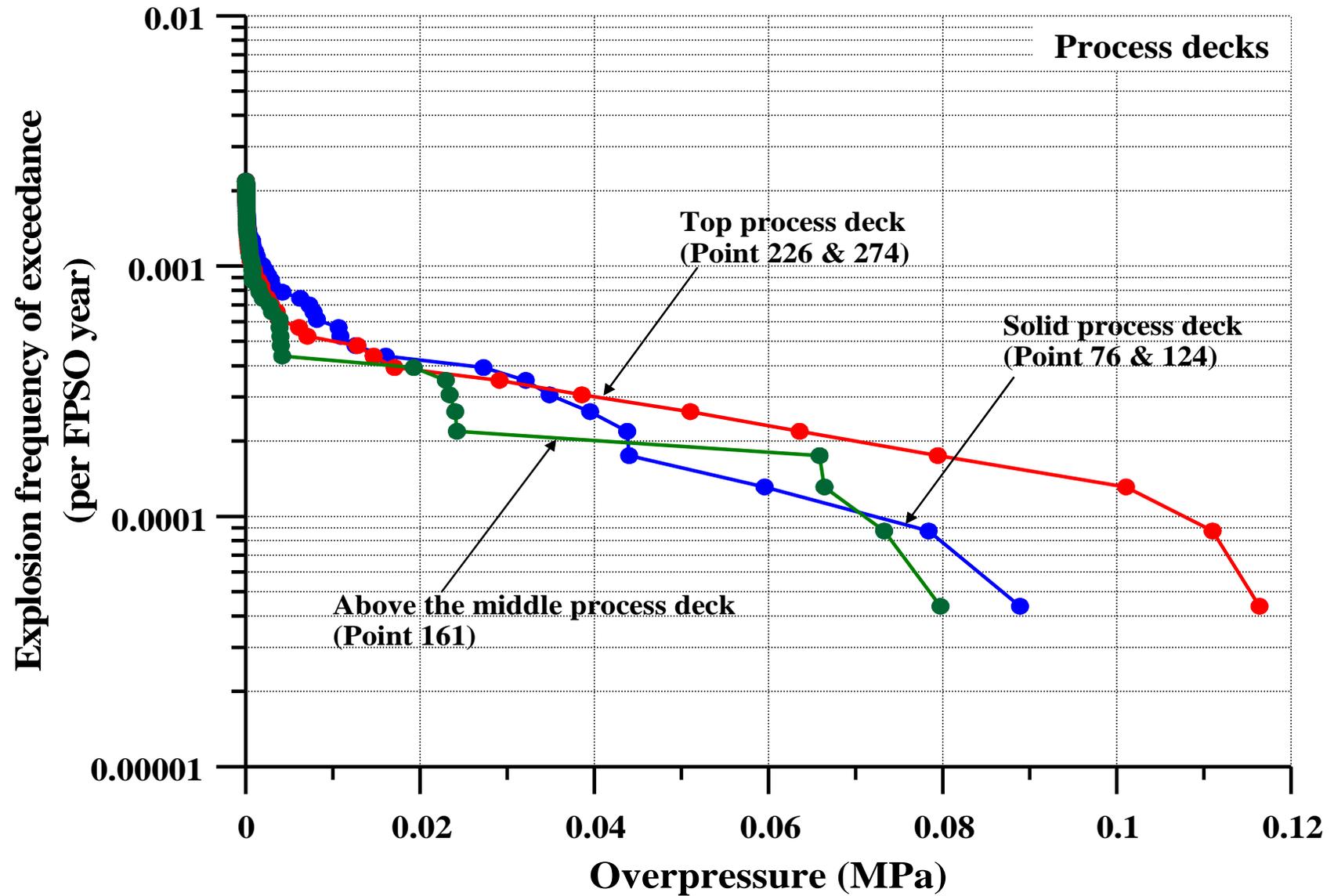
# Applied Example: VLCC Class FPSO Topsides



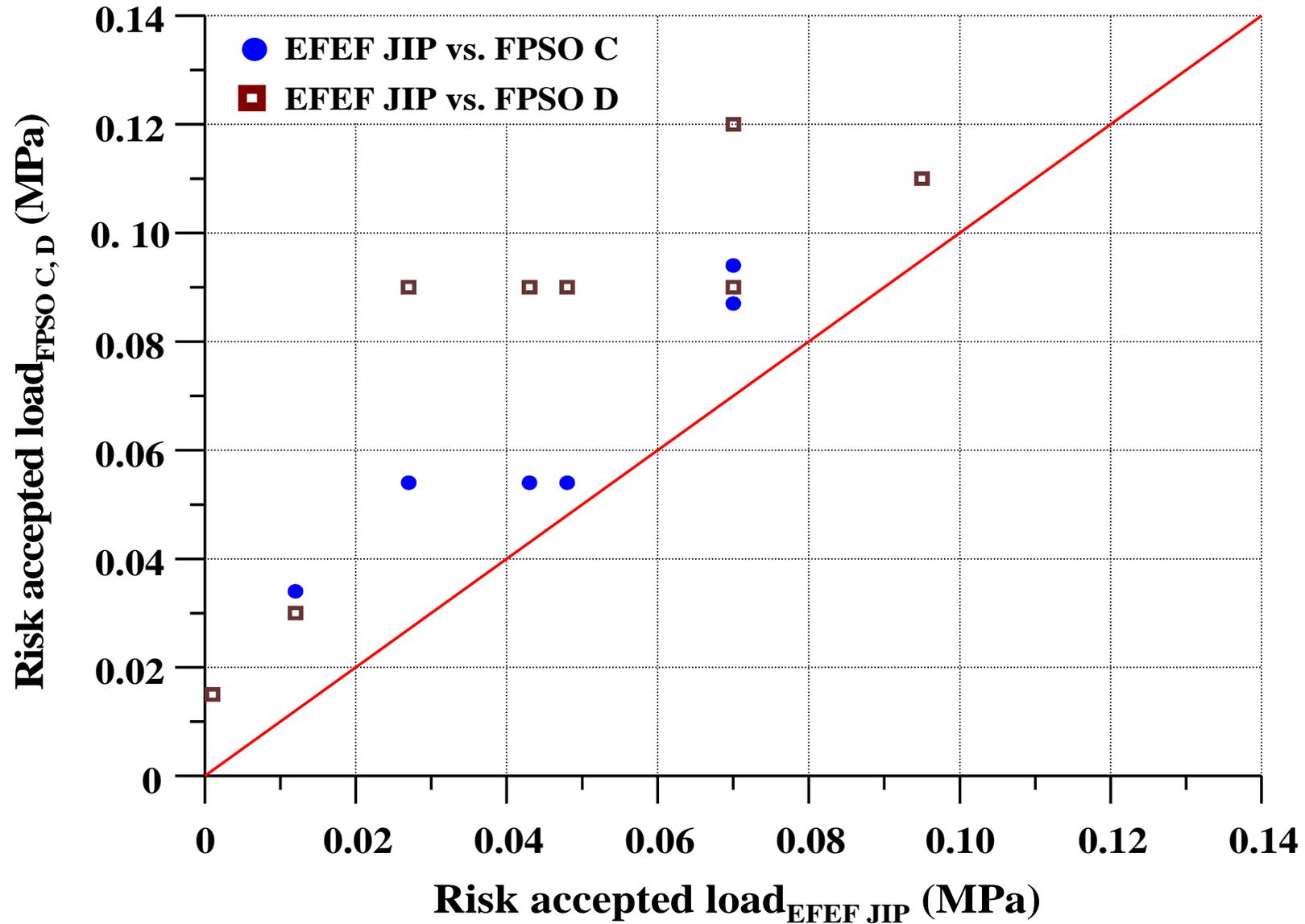
## Effect of Gas Cloud Volume on Maximum Overpressure – Comparison between EFEF JIP and Existing FPSO Practices



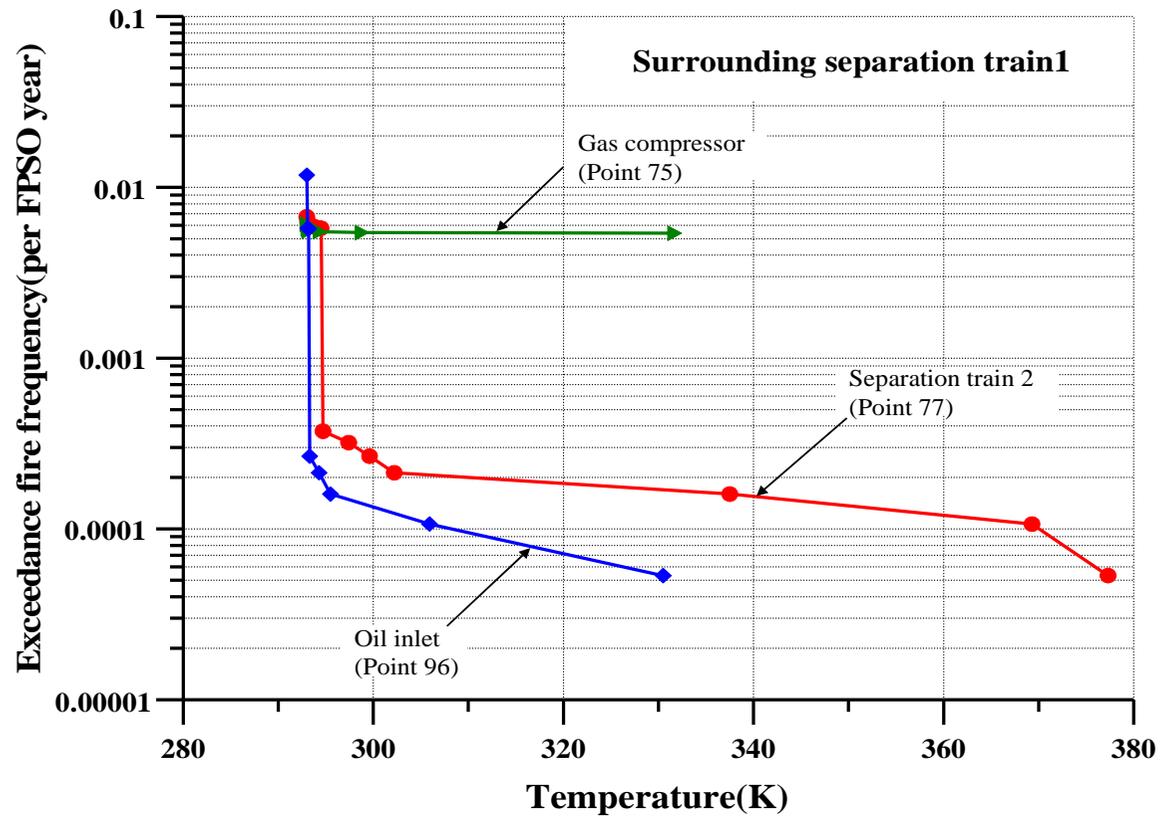
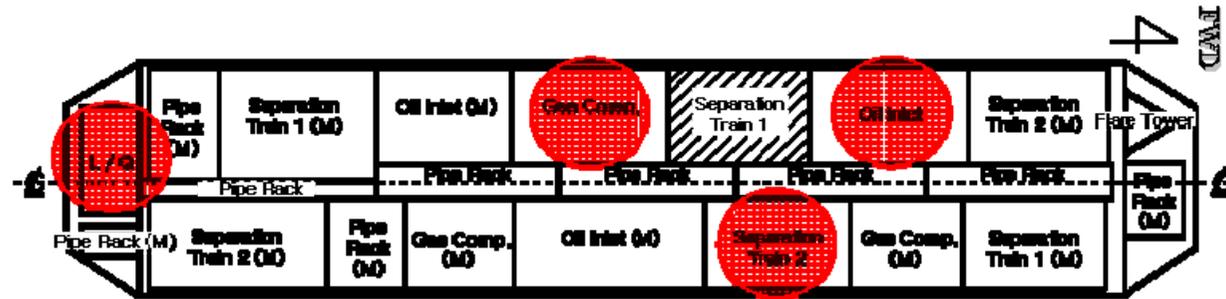
# Design Explosion Loads with Exceedance Curves



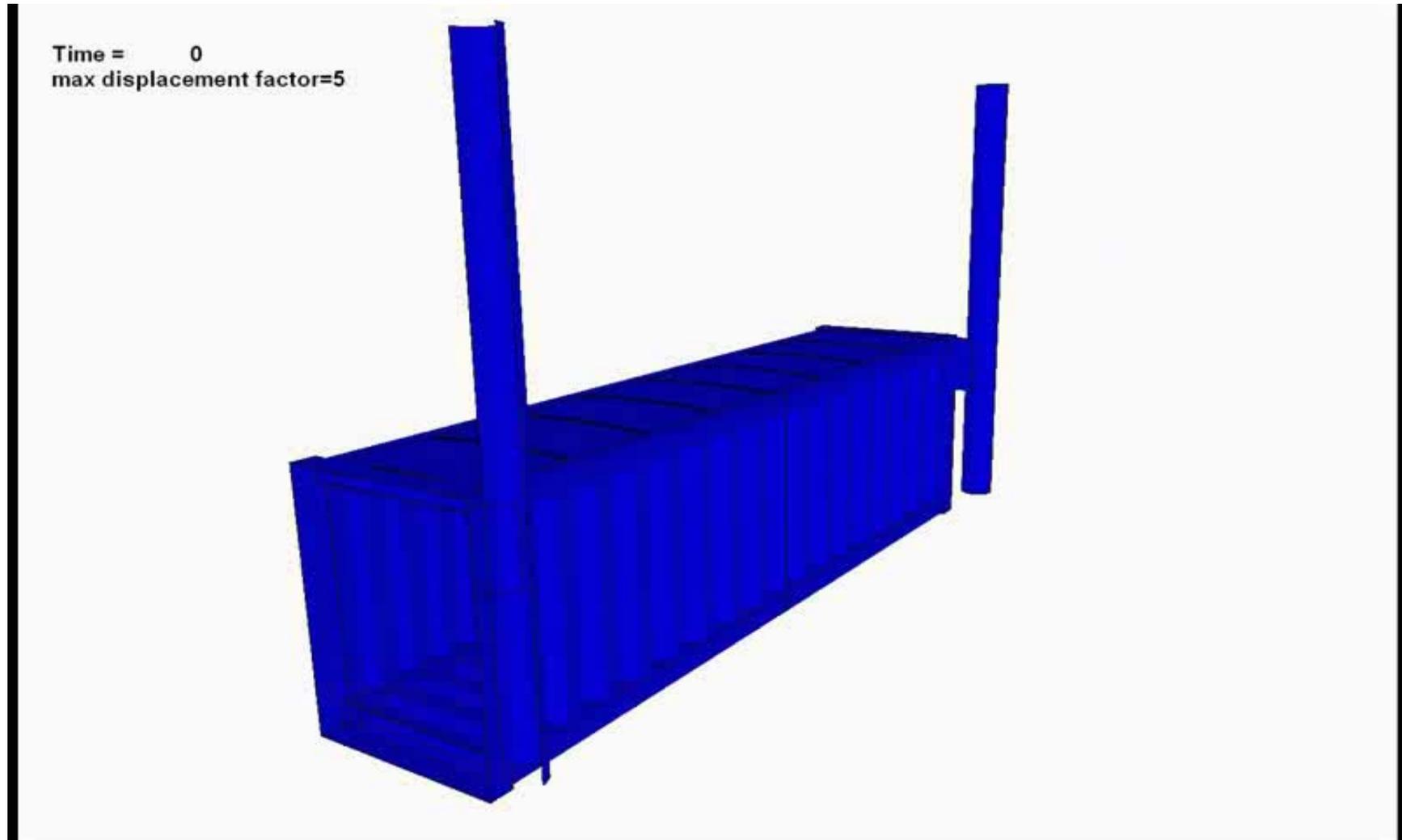
# Design Explosion Loads – Comparison between EFEF JIP and Existing FPSO Practices



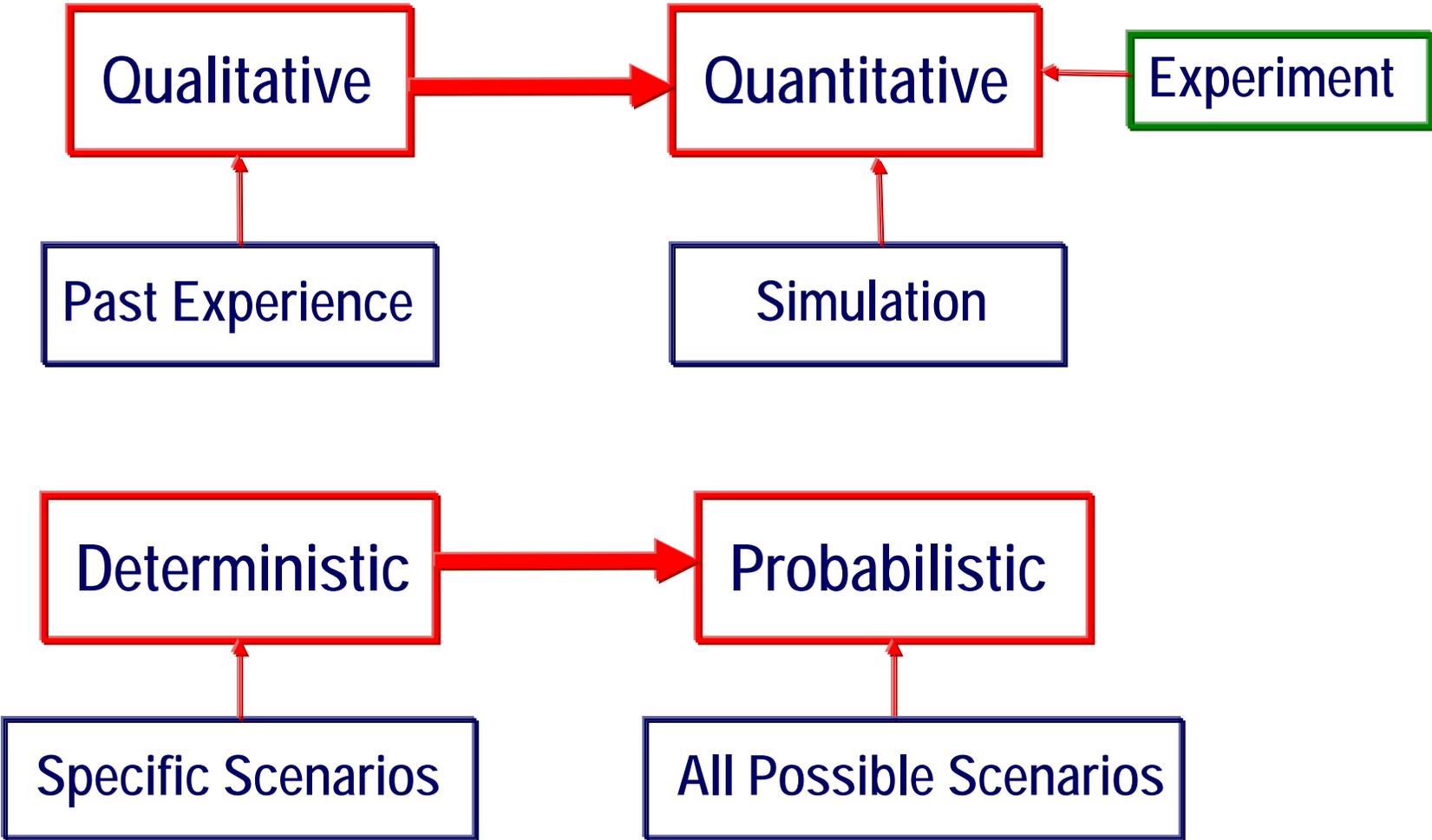
# Design Fire Loads with Exceedance Curves



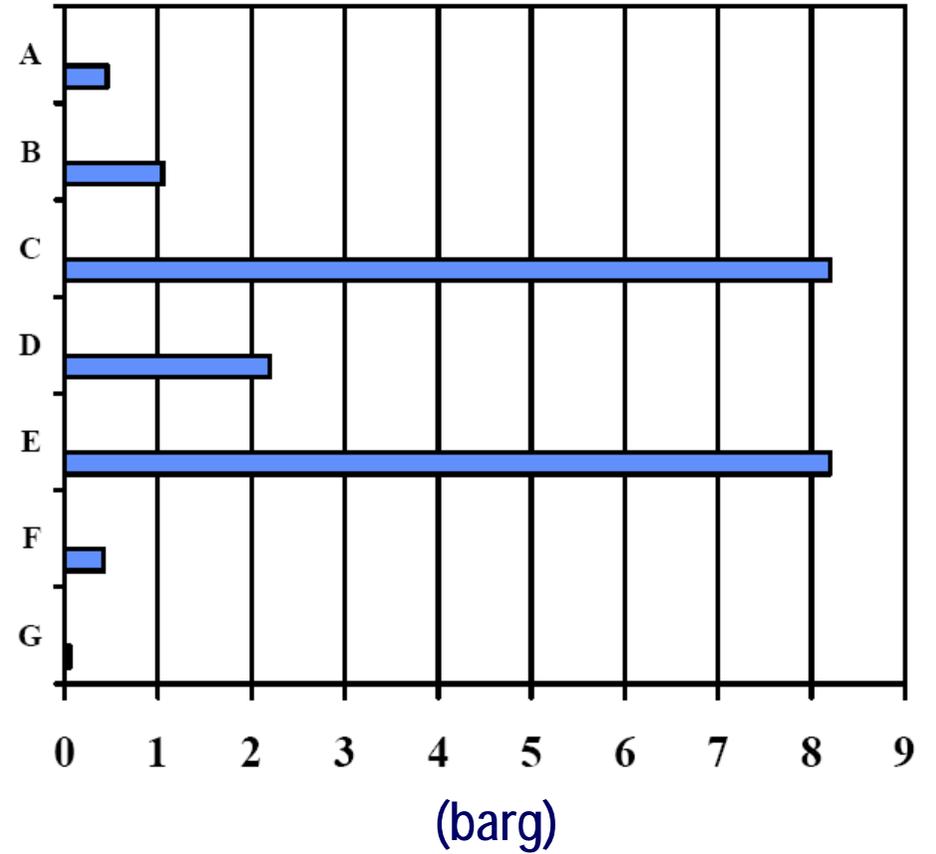
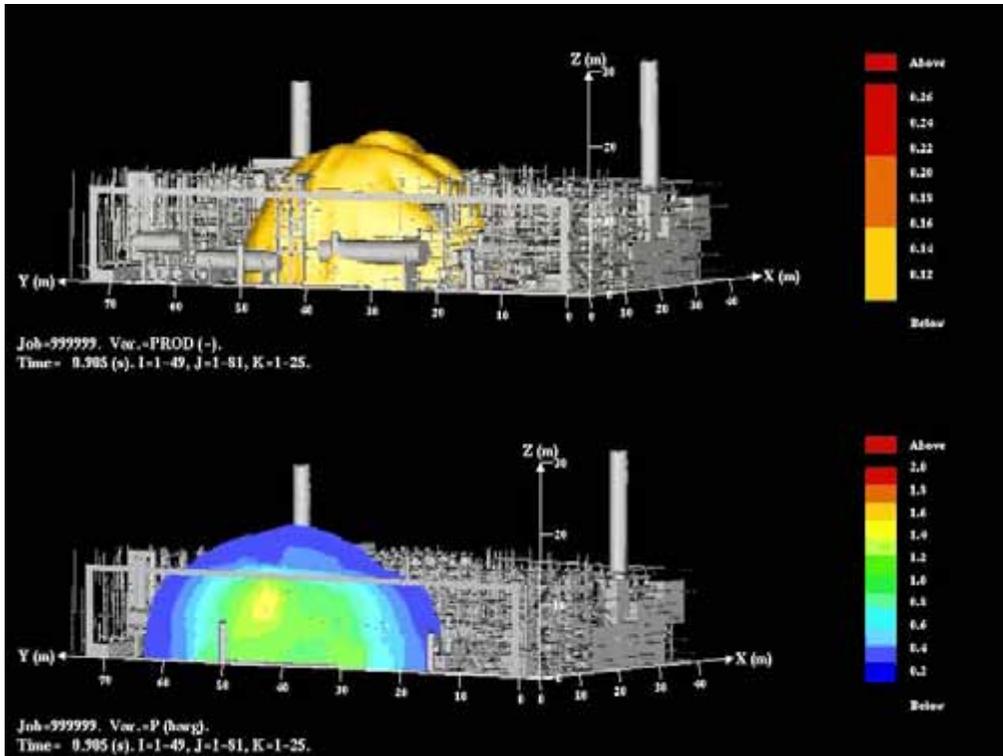
# Nonlinear Structural Consequence Analysis – Escape Route



# Trends in Risk Assessment



# CFD Explosion Simulations



# Gas Explosion Tests with or without Water Sprays (1/2)

## - Importance of Risk Management



Without water sprays

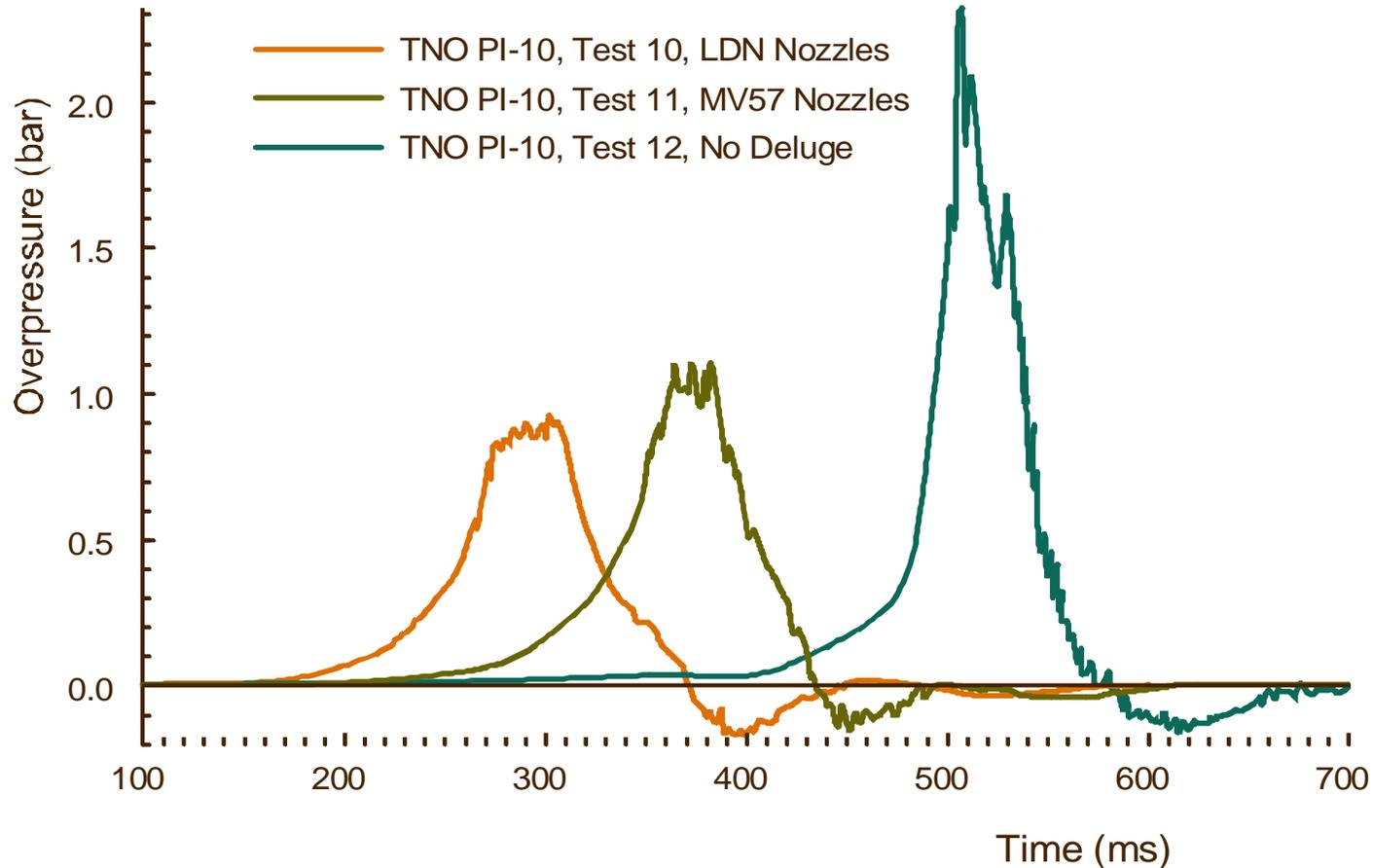


With water sprays

Source: © The Steel Construction Institute, Fire and Blast Information Group

# Gas Explosion Tests with or without Water Sprays (2/2)

## - Importance of Risk Management



Source: © The Steel Construction Institute, Fire and Blast Information Group

# Explosion and Fire Test Facilities under Construction in Korea

